

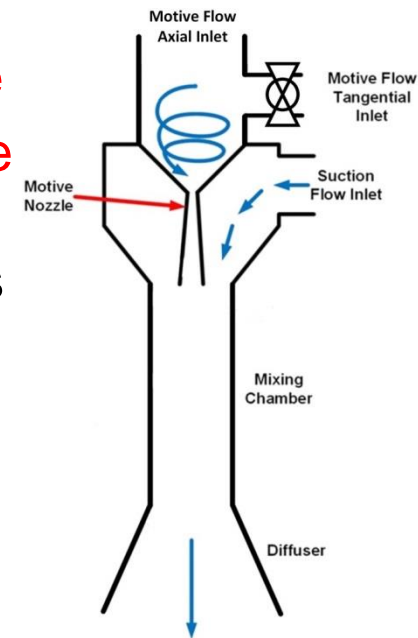
A NEW CONTROL MECHANISM FOR TWO-PHASE EJECTOR IN VAPOR COMPRESSION CYCLES FOR AUTOMOTIVE APPLICATIONS USING ADJUSTABLE MOTIVE NOZZLE INLET SWIRL

Jingwei Zhu, Stefan Elbel

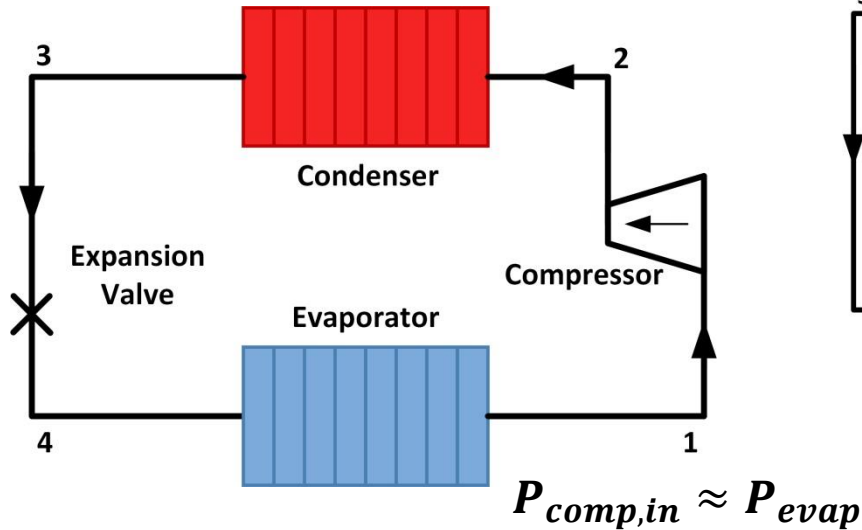
University of Illinois at Urbana-Champaign
Department of Mechanical Science and Engineering
Air Conditioning and Refrigeration Center (ACRC)



- Background: opportunities and challenges with ejector cooling cycles
- Research motivation: optimize ejector cycle performance under changing working conditions/capacities (common in automotive applications) by **adjusting ejector motive nozzle**
- New solution: swirl ejector - utilizing **controllable swirl at the motive inlet of the ejector** to adjust mass flow rate and condenser outlet quality/subcooling (**Swirl nozzle/valve** has been recognized as a reliable flow modulation method as early as 1960s (Mayer, 1967; Wormley, 1969))
- Research approach:
 - Swirl nozzle tests with refrigerant (R134a)
 - Visualization and modeling of low-quality flow expanded in the nozzle
- Conclusions

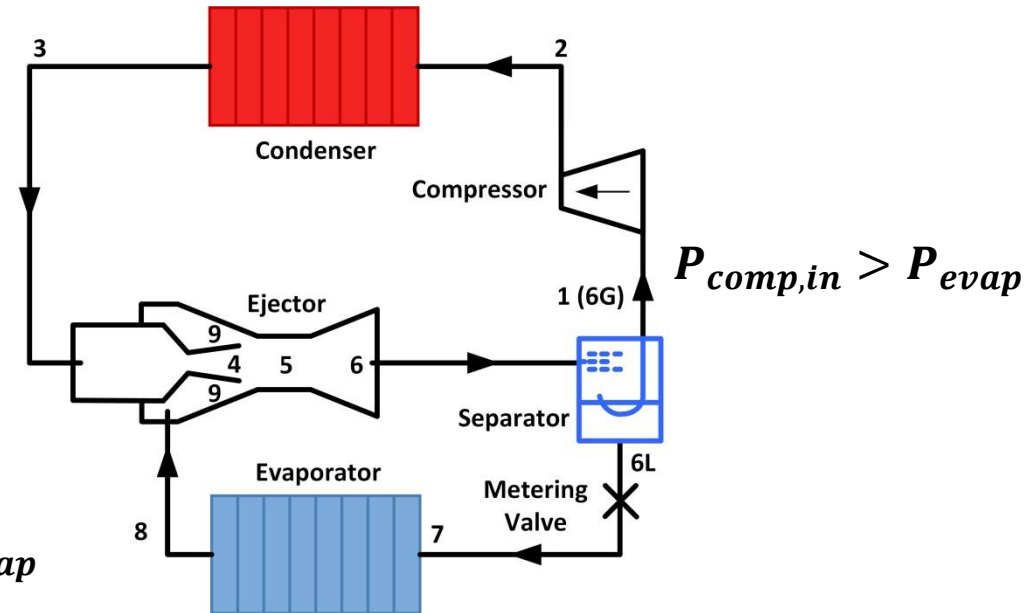


Benefits of Ejector Cooling Cycles



Conventional cooling cycle:

- Throttling in the expansion valve causes irreversibility
- Cycle efficiency is impaired



Ejector cooling cycle:

- Irreversibility in the expansion process is reduced
- Compressor work is saved
- Cooling capacity is increased
- Cycle efficiency is improved
(R134a ~ 5 %; CO₂ ~ 20 %)

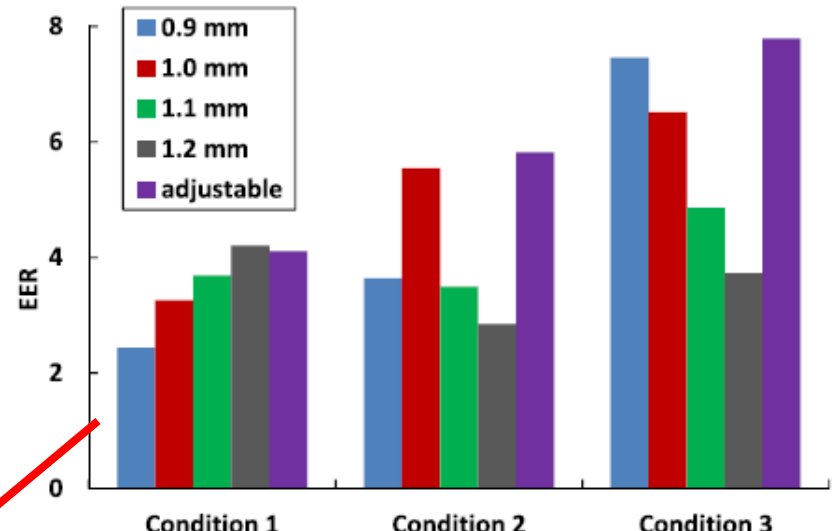
- Different working conditions/capacities favor different ejector geometry
Elbel and Hrnjak (2008); Elbel (2011);

	Condition 1	Condition 2	Condition 3
T_{indoor} (dry/wet bulb), °C	26.7/19.4	26.7/19.4	26.8/19.5
$T_{outdoor}$ (dry/wet bulb), °C	35.0/19.5	30.6/16.8	27.8/14.9
p_{cond} , MPa	2.4	2.0	1.9

- Slightly different geometry might result in significant difference in system COP under the same conditions
Sumeru *et al.* (2012); Sarkar (2012);

- Ejector motive nozzle throat diameter (nozzle restrictiveness) is one of the key points that can significantly affect COP
COP changed by more than 40 %

Test Conditions



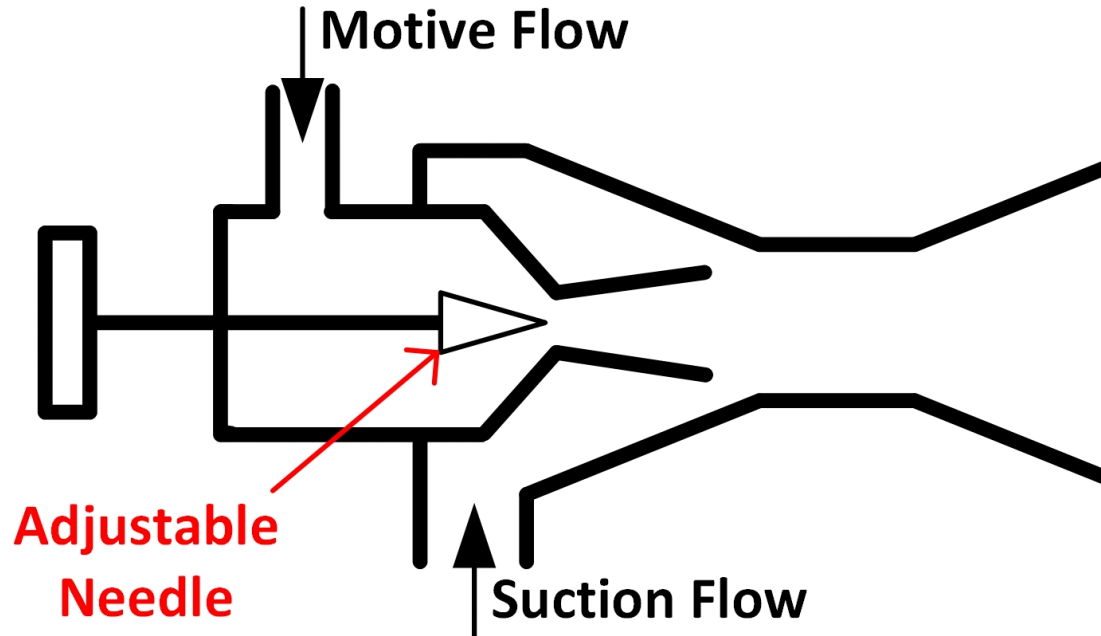
R410A ejector air conditioning system COP with different motive nozzle throat diameters under three different conditions
Hu *et al.* (2014)

How to Adjust Motive Nozzle Geometry (Restrictiveness on Flow)



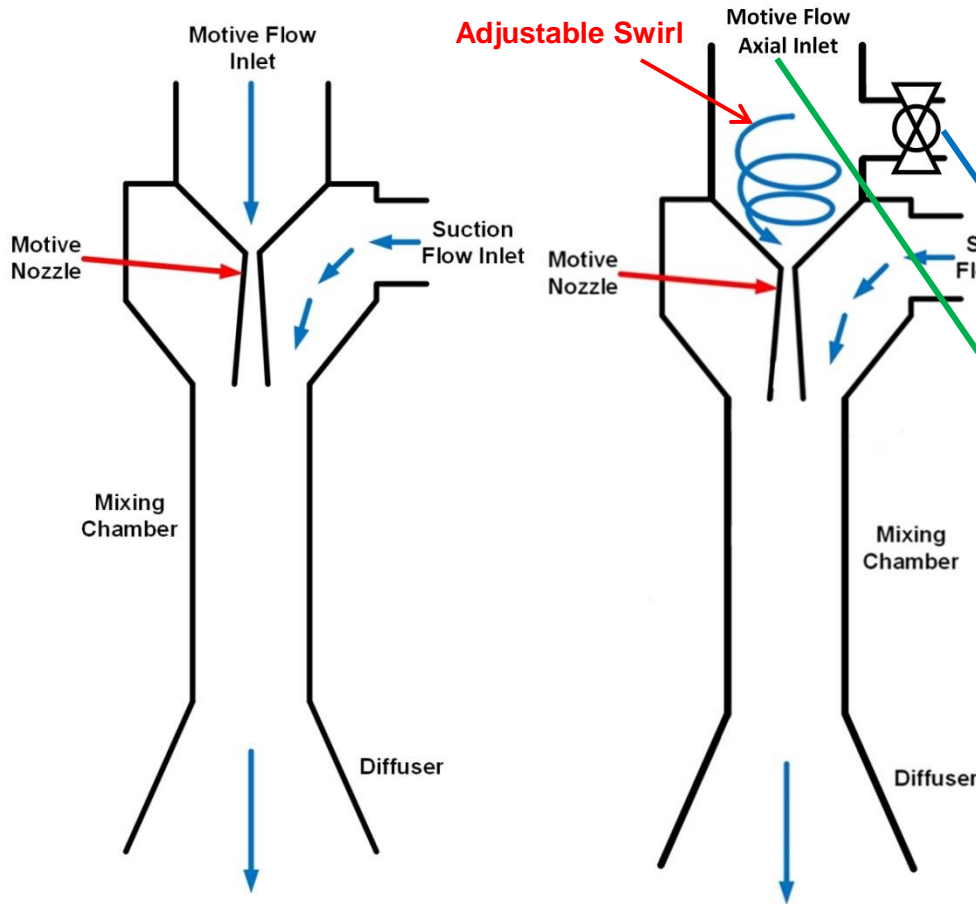
Eurofighter Typhoon thrust nozzle

<http://www.military.com/video/aircraft/engines/eurofighter-thrust-vectoring-nozzle/2907034546001>



This design is complicated and costly, and more friction losses are incurred because of the additional surface area and turbulence introduced.

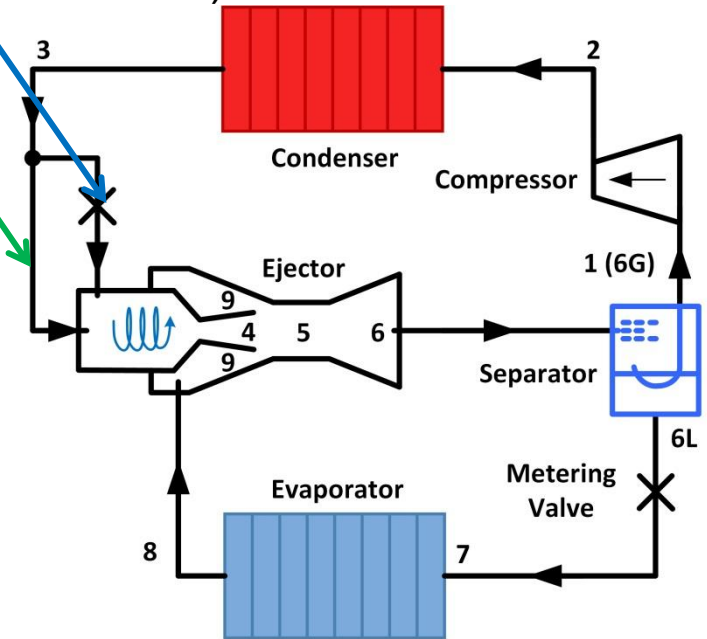
New Solution: Swirl Ejector



Conventional ejector

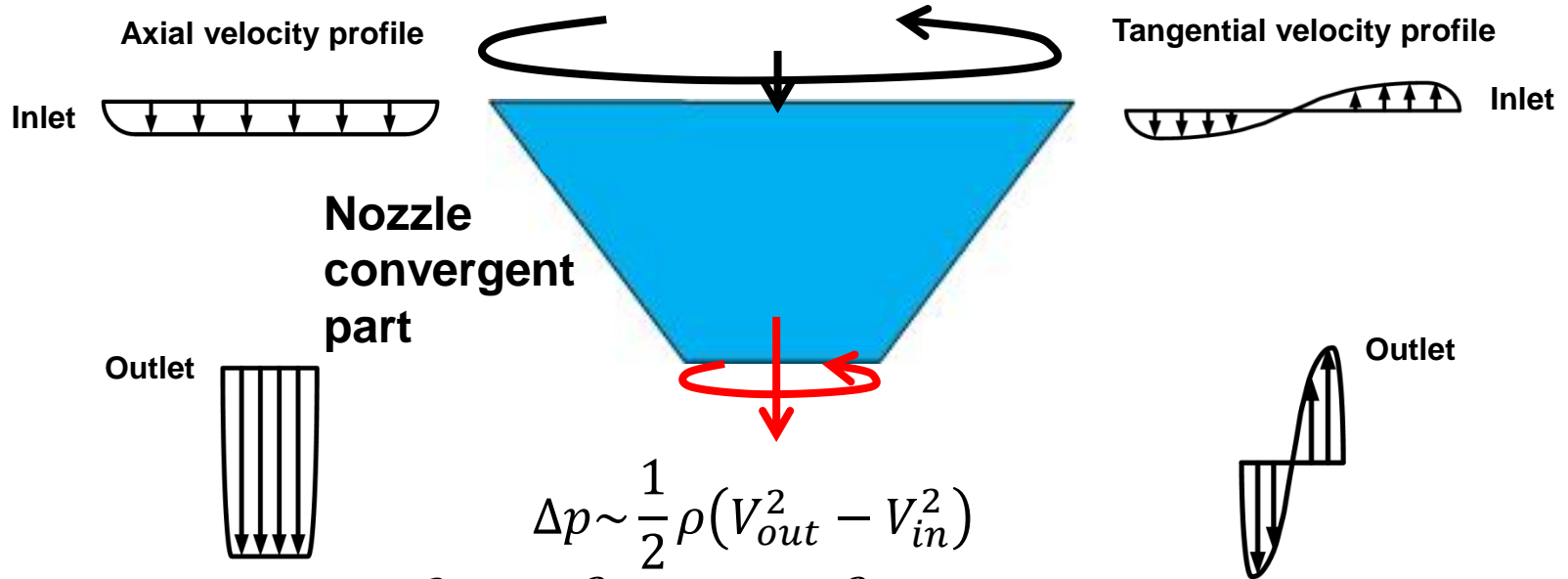
Swirl ejector

Utilizing an adjustable swirl at the motive inlet to control the flow expanded in the motive nozzle (no change in geometry; same effect as changing nozzle throat diameter)



Swirl ejector cooling cycle

Hypothesis 1: Share of Tangential Kinetic Energy in the Available Pressure Potential Decreases the Mass Flow Rate



$$\Delta p \sim \frac{1}{2} \rho (V_{out}^2 - V_{in}^2)$$

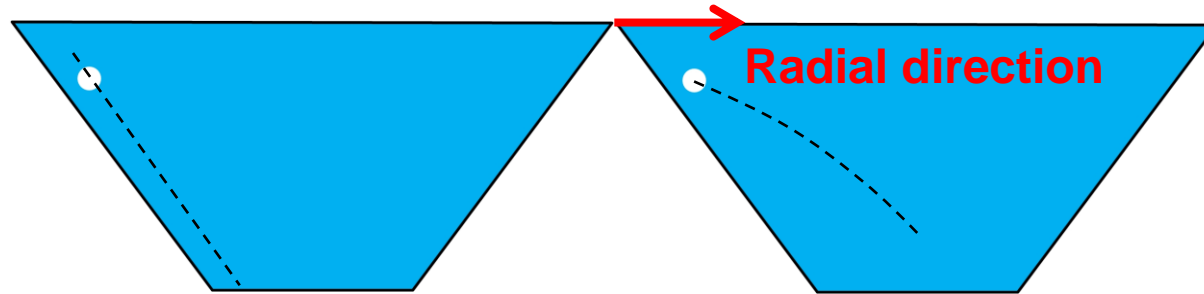
$$V_{out}^2 = V_{axial,out}^2 + V_{tangential,out}^2$$

$$\dot{m} \sim \rho V_{axial,out} A_{out}$$

Works for both single-phase and two-phase

Hypothesis 2: Swirl Boosts Vapor Bubble Growth

**Nozzle
convergent
part**



No Swirl

With stronger swirl, more relative motion is created between bubbles and surrounding liquid in radial direction

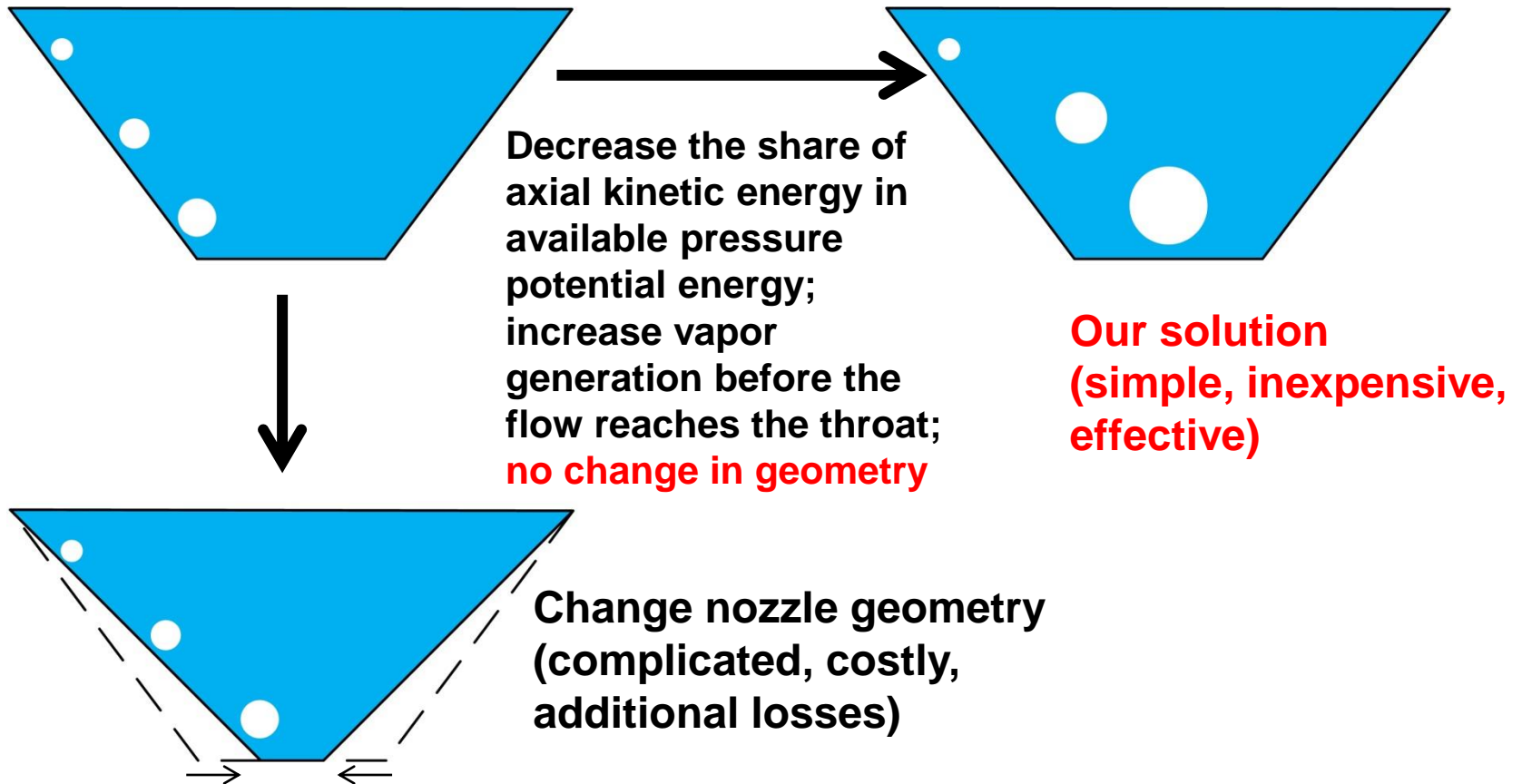
- Two-phase flow during expansion is usually not in equilibrium (Bubble growth takes time)

$$\frac{d(m_{bubble})}{dt} h_{lv} = 4\pi R_{bubble}^2 \bar{h} (T_{liquid,\infty} - T_s)$$

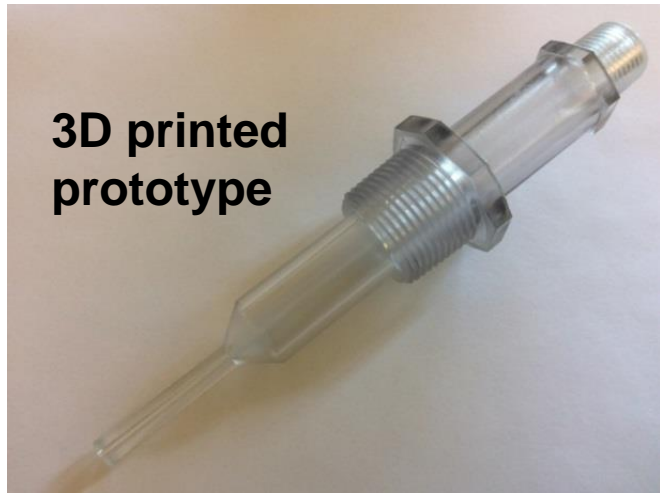
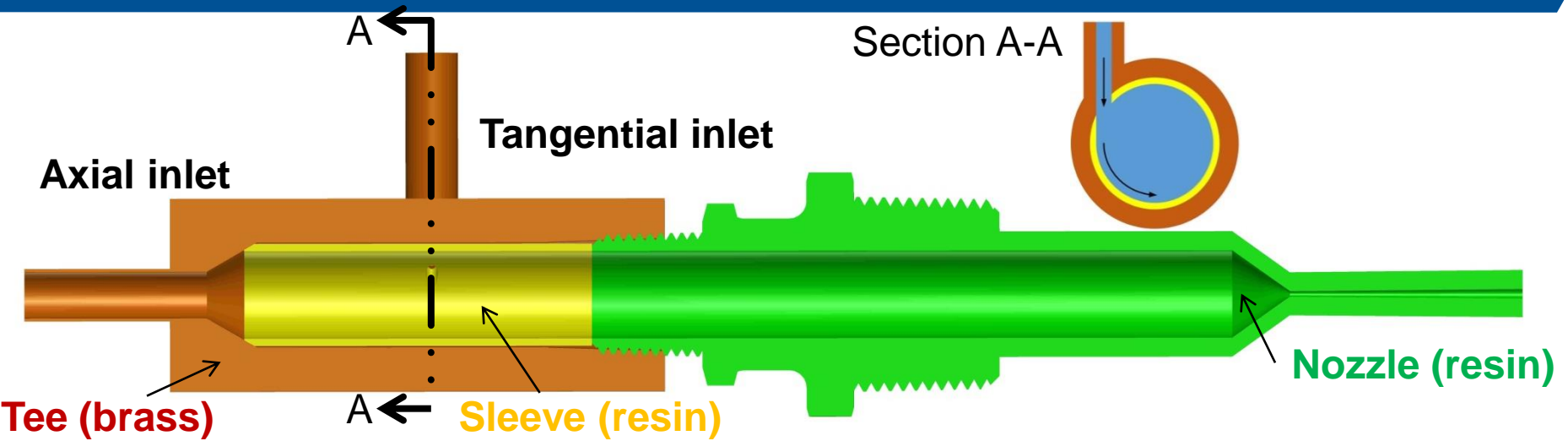
$$\overline{Nu}_{sphere} = \frac{\bar{h} D_{bubble}}{k} = 2 + [0.4 Re^{\frac{1}{2}} + 0.06 Re^{\frac{2}{3}}] Pr^{0.4} \left(\frac{\mu_{liquid,\infty}}{\mu_{liquid,s}} \right)^{\frac{1}{4}} \quad Re \sim V_{relative}$$

- The stronger the swirl is the faster bubbles grow
- **Works for two-phase flow**

How to Make Nozzle Have More Restrictiveness on The Two-Phase Flow?



- **Experimental investigation** of the influence of motive inlet swirl on the flow expanded in the motive nozzle with commonly used refrigerant R134a
- **Visualization** of the swirling flow expanded in the nozzle
- **Explanation and modeling** of the influence of motive inlet swirl on the flow expanded in the motive nozzle (ongoing)
- **Evaluation of the nozzle efficiency** with swirl control and **comparison** with other control methods; **system tests** with adjustable swirl ejector under different working conditions in the future



3D printed prototype

Nozzle inlet diameter (mm)	15.0
Nozzle throat diameter (mm)	1.0
Nozzle outlet diameter (mm)	1.7
Nozzle convergent part length (mm)	9.9
Nozzle divergent part length (mm)	40.0
Tangential inlet inner diameter (mm)	2.0
Swirl decay distance (mm)	138.0

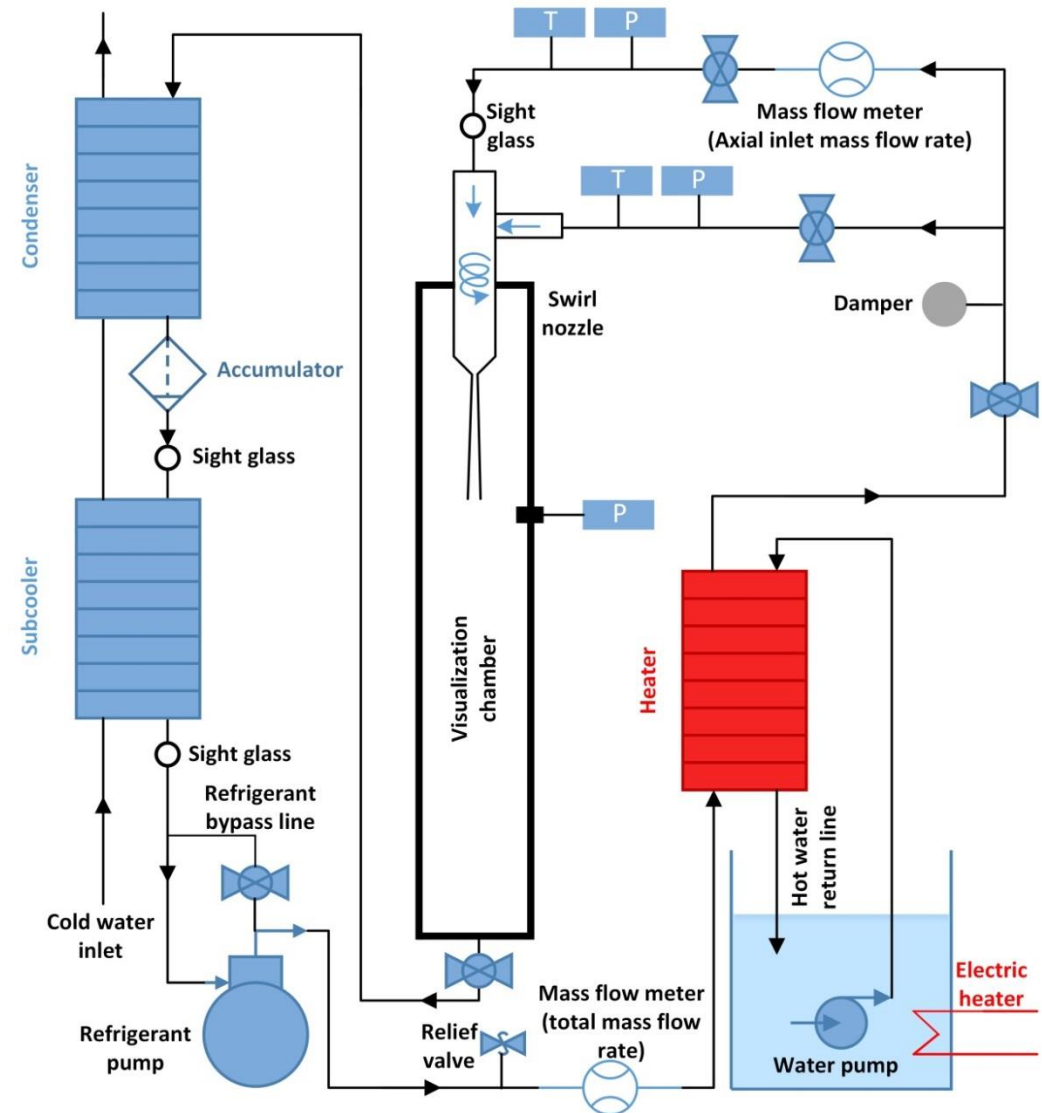
Convergent-divergent nozzle (resin)

Swirl nozzle geometry

Experimental Facility for Investigation of Swirl Influence on Nozzle Restrictiveness

- Pumped-refrigerant-loop for adjustment of nozzle test conditions
- Pressures and temperatures at the axial and tangential inlets are measured; pressure at the nozzle outlet is measured
- Total mass flow rate and axial inlet mass flow rate are measured by Coriolis flow meters
- Ratio of tangential inlet mass flow rate to total mass flow rate is adjusted by two valves

$$\text{Swirl strength} = \frac{\dot{m}_{\text{tangential}}}{\dot{m}_{\text{total}}}$$

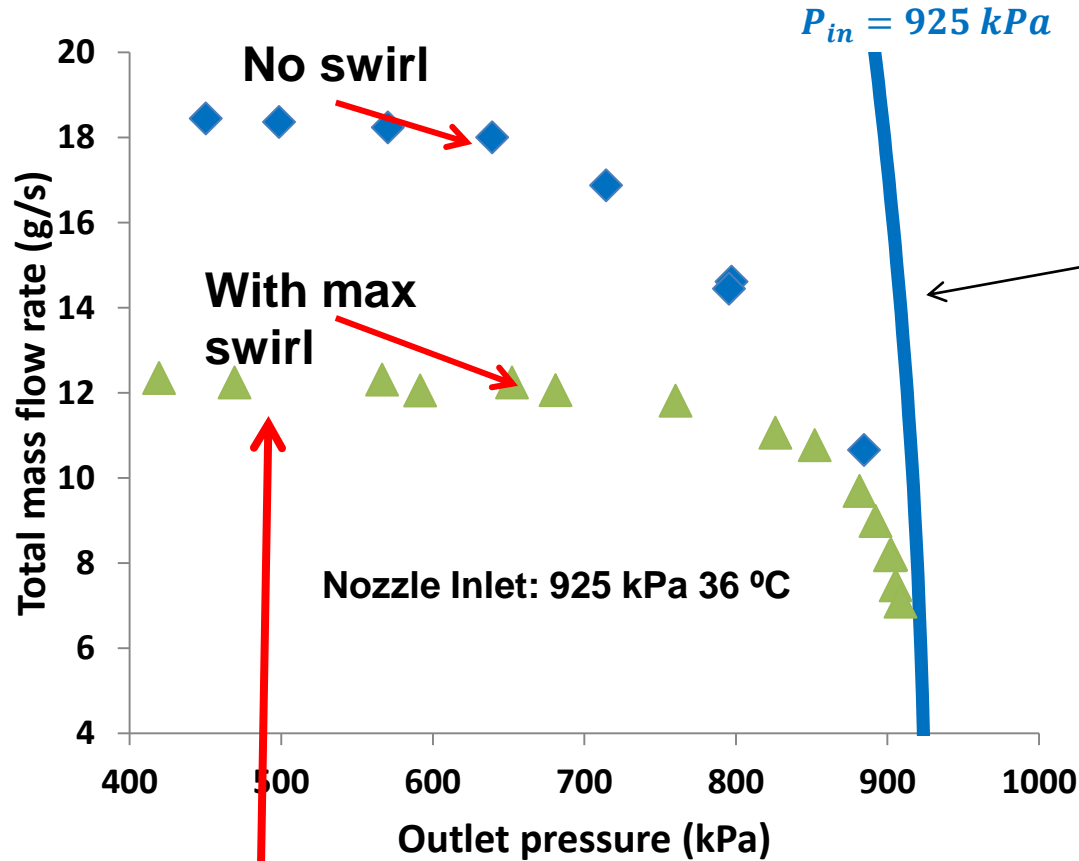


- Working fluid: R134a
- Different nozzle inlet pressures are achieved by adjusting the heating water temperature and pump speed
- Nozzle outlet pressure can be adjusted by a valve installed in the downstream of the nozzle
- Flow at the nozzle inlet is subcooled by around 0.5 °C. No observable bubbles at the nozzle inlet (guaranteed by observing through the sight glass installed at the nozzle inlet).

Test Matrix

P_{in} (kPa)	P_{out} (kPa)	T_{in} (°C)	\dot{m}_{total} (g/s)	Vortex strength (-)
760~1059	407~909	29~41	6~20	0~1

Effect of Outlet Pressure on Nozzle Mass Flow Rate at Constant Inlet Pressure



Inlet subcooling = 0.5 °C

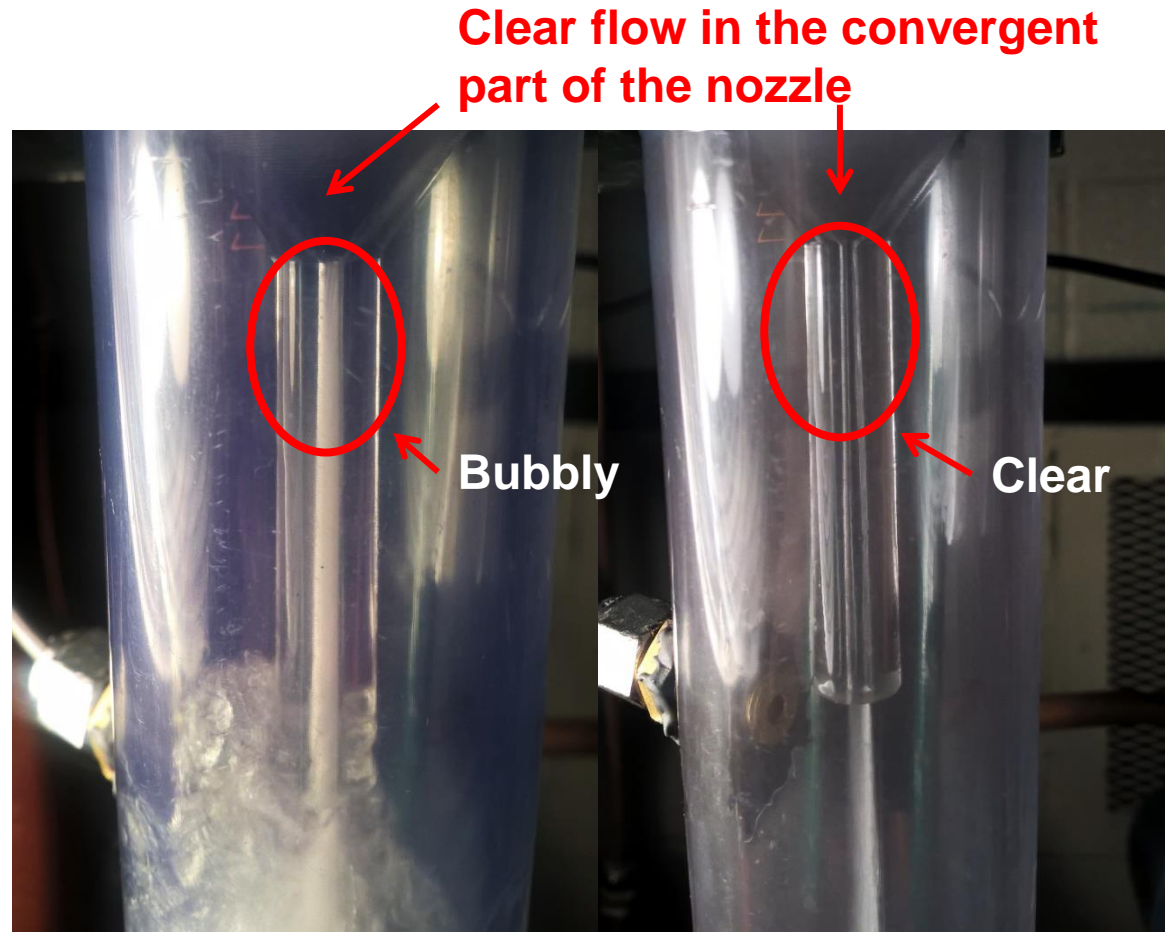
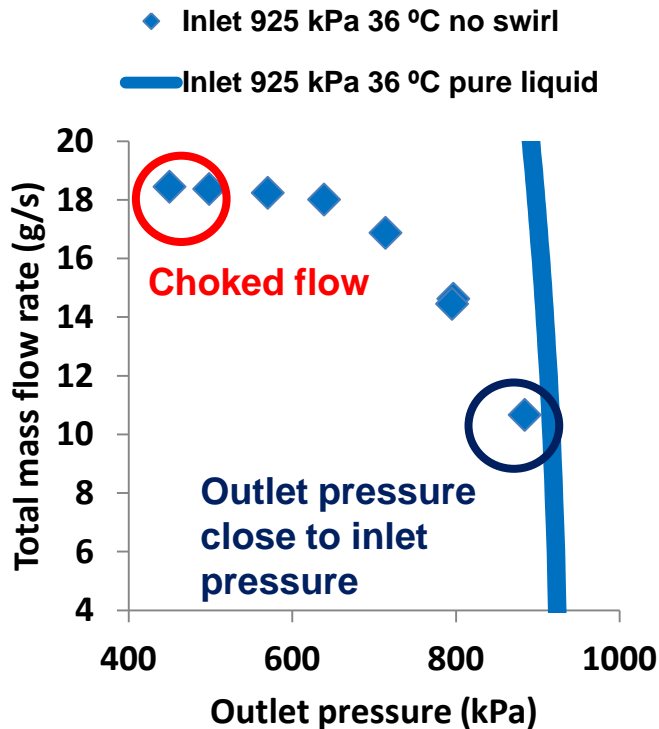
Theoretically calculated incompressible single phase liquid mass flow rate

Observations:

- Flow is choked at low outlet pressure
- Inlet swirl reduces total mass flow rate under the same inlet and outlet conditions (**larger restrictiveness**)

**Choked at low outlet pressure
(decrease in outlet pressure does not increase mass flow rate)**

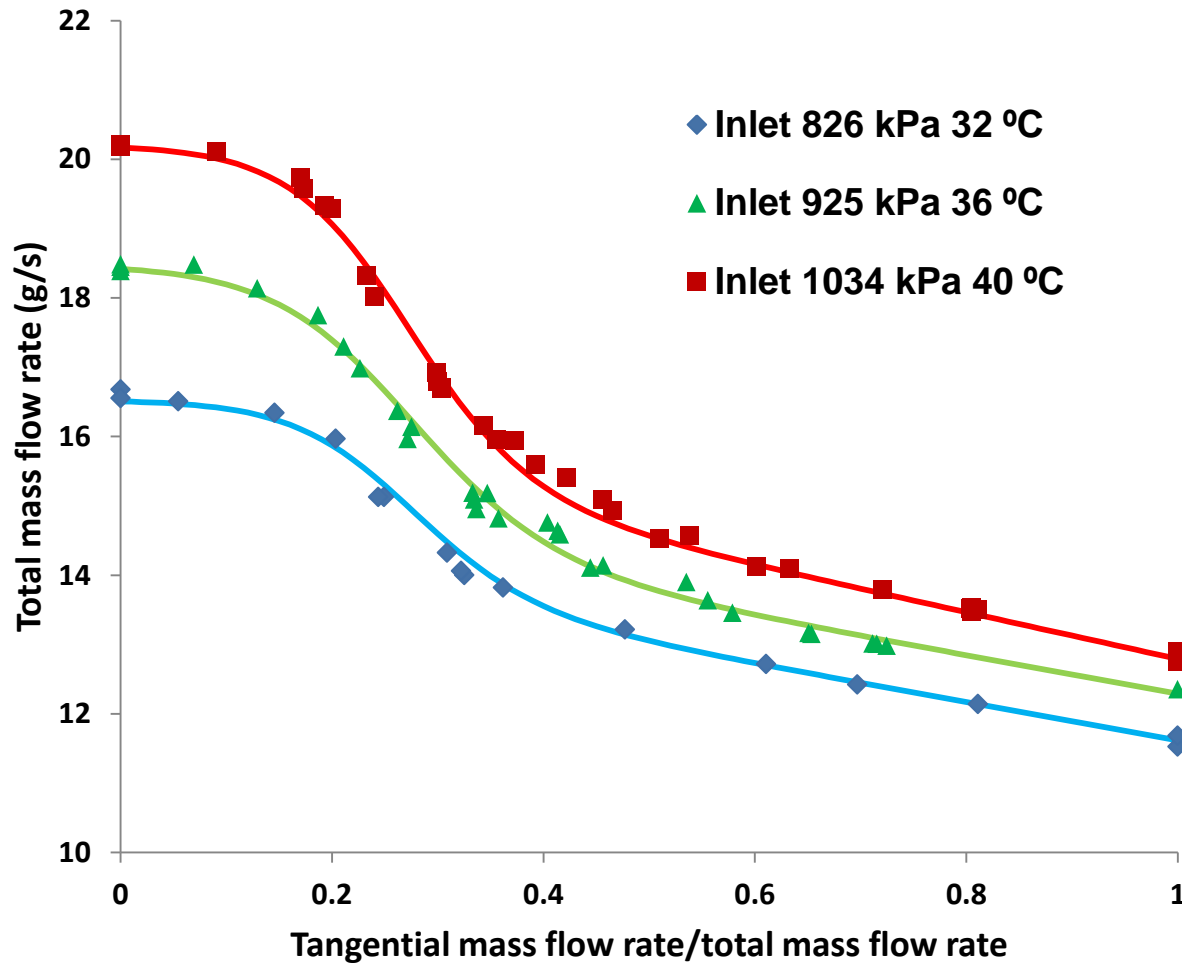
Preliminary Visualization Results



Choked flow (very low outlet pressure): becomes **bubbly** immediately after the throat

Outlet pressure close to inlet pressure: flow is still **clear** after the throat

Choked Mass Flow Rate with Different Inlet Swirl Strengths at Constant Inlet Pressure

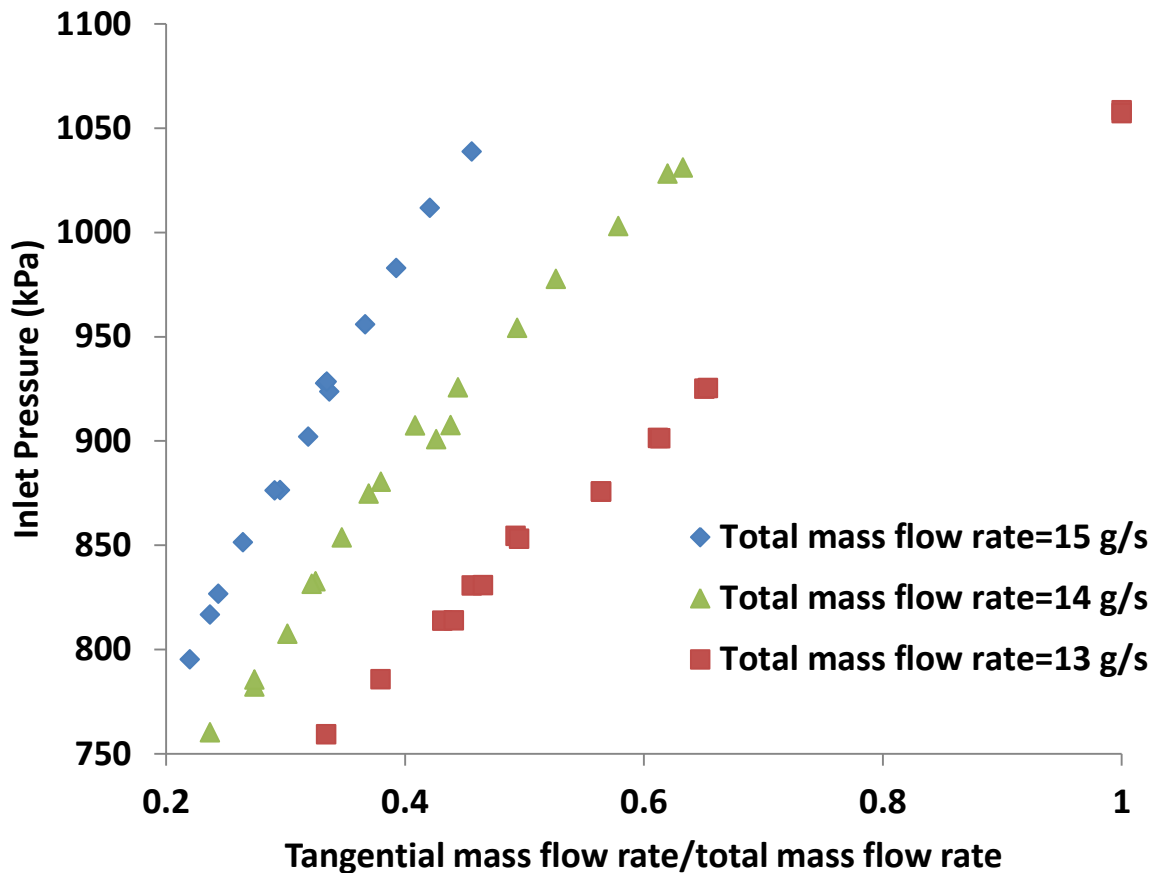


Inlet subcooling = 0.5 °C

Mass flow rate can be reduced by 35 % with swirl under the same inlet and outlet conditions (large control range).
Nozzle

restrictiveness on the flow is changed by swirl; the stronger the swirl is, the larger the restrictiveness is.

Nozzle Inlet Pressure Can Vary in A Wide Range with Different Inlet Swirl Strengths at Constant Total Mass Flow Rate



■ Inlet subcooling = 0.5 °C

Mass flow rate ratio (swirl strength): 0.2 to 0.5

Inlet pressure: 780 kPa to 1050 kPa (large control range) for total mass flow rate = 15 g/s

Nozzle restrictiveness on the flow is changed by swirl; the stronger the swirl is, the larger the restrictiveness is.

- Nozzle inlet swirl can change nozzle restrictiveness on the two-phase flow. The stronger the swirl is, the larger the restrictiveness is.
- The control range of inlet pressure and mass flow rate is large enough for real applications. Mass flow rate can be reduced by **35 %** with swirl under the same nozzle inlet and outlet conditions.
- Next step: Compare the efficiency of swirl ejector with other control methods to see if it reduces the frictional losses for the same range of flow control.
- Goal: By adjusting the restrictiveness of motive nozzle on the flow expanded through it, ejector cycle performance can be optimized for different working conditions/capacities and the improvements could be more than 40 %.

Thank you for your attention!
Any questions?

- Presenter: Jingwei Zhu
- Email: jzhu50@illinois.edu
- Acknowledgments: The authors would like to thank the member companies of the Air Conditioning and Refrigeration Center at the University of Illinois at Urbana-Champaign for their generous support.

1. Gay, N. H., "Refrigerating System," U.S. Patent 1,836,318, 1931.
2. Disawas, S. and Wongwises, S., "Experimental investigation on the performance of the refrigeration cycle using a two-phase ejector as an expansion device," *International Journal of Refrigeration*, 27(6): 587-594, 2004.
3. Lawrence, N., and Elbel, S., "Experimental and Numerical Study on the Performance of R410A Liquid Recirculation Cycles with and without Ejectors," 15th International Refrigeration and Air Conditioning Conference at Purdue, West Lafayette, IN, USA, Paper 2187, 2014.
4. Ozaki, Y., Takeuchi, H., and Hirata, T., "Regeneration of expansion energy by ejector in CO₂ cycle," 6th IIR Gustav Lorentzen Conference on Natural Working Fluid, Glasgow, UK, 11-20, 2004.
5. Banasiak, K., Hafner, A., and Andresen, T., "Experimental and numerical investigation of the influence of the two-phase ejector geometry on the performance of the R744 heat pump," *International Journal of Refrigeration*, 35(6): 1617-1625, 2012.
6. **Elbel, S. and Hrnjak, P., "Experimental validation of a prototype ejector designed to reduce throttling losses encountered in transcritical R744 system operation," *International Journal of Refrigeration*, 31(3): 411-422, 2008.**
7. **Elbel, S., "Historical and present developments of ejector refrigeration systems with emphasis on transcritical carbon dioxide air-conditioning applications," *International Journal of Refrigeration*, 34(7): 1545-1561, 2011.**
8. Harrell, G. S., and Kornhauser, A. A., "Performance tests of a two-phase ejector," American Society of Mechanical Engineers, New York, NY, United States, 1995.
9. Lawrence, N. and Elbel S., "Experimental investigation of a two-phase ejector cycle suitable for use with low-pressure refrigerants R134a and R1234yf," *International Journal of Refrigeration*, 38: 310-322, 2014.

10. Sumeru, K., Nasution, H., and Ani, F. N., “A review on two-phase ejector as an expansion device in vapor compression refrigeration cycle,” *Renewable and Sustainable Energy Reviews*, 16(7): 4927-4937, 2012.
11. Sarkar, J., “Ejector enhanced vapor compression refrigeration and heat pump systems - A review,” *Renewable and Sustainable Energy Reviews*, 16(9): 6647-6659, 2012.
12. Hu, J., Shi, J., Liang, Y., Yang, Z., and Chen, J., “Numerical and experimental investigation on nozzle parameters for R410A ejector air conditioning system,” *International Journal of Refrigeration*, 40: 338-346, 2014.
13. Henry, R. E., and Fauske, H. K., “The two-phase critical flow of one-component mixtures in nozzles, orifices, and short tubes,” *Journal of Heat Transfer*, 93(2): 179-187, 1971.
14. Schrock, V. E., Starkman, E. S., and Brown, R. A., “Flashing flow of initially subcooled water in convergent–divergent nozzles,” *Journal of Heat Transfer*, 99(2): 263-268, 1977.
15. Plesset, M. S., and Zwick, S. A., “The growth of vapor bubbles in superheated liquids,” *Journal of Applied Physics*, 25(4): 493-500, 1954.
16. Florschuetz, L. W., Henry, C. L., and Khan, A. R., “Growth rates of free vapor bubbles in liquids at uniform superheats under normal and zero gravity conditions,” *International Journal of Heat and Mass Transfer*, 12(11): 1465-1489, 1969.
17. Ruckenstein, E., and Davis, E. J., “The effects of bubble translation on vapor bubble growth in a superheated liquid,” *International Journal of Heat and Mass Transfer*, 14(7): 939-952, 1971.
18. Mayer, E. A., “Large-signal vortex valve analysis,” *Advances in Fluidics*, 233-249, 1967.
19. Wormley, D. N., “An analytical model for the incompressible flow in short vortex chambers,” *Journal of Basic Engineering*, 91(2): 264-272, 1969.