Ideal Gas Thermodynamic Properties in Chemkin Format

Thermodynamic properties for ideal gases are tabulated in a variety of locations in Chemkin format. This format involves two sets of seven constants a_1 through a_7 . These constants are fits to specific heat, enthalpy, and entropy data (or calculations) according to the following formulae:

$$\frac{\hat{c_p}}{R_u} = \frac{c_p}{R} = a_1 + a_2 T + a_3 T^2 + a_4 T^3 + a_5 T^4 \tag{1}$$

$$\frac{\hat{h}}{R_n T} = \frac{h}{RT} = a_1 + \frac{a_2}{2}T + \frac{a_3}{3}T^2 + \frac{a_4}{4}T^3 + \frac{a_5}{5}T^4 + \frac{a_6}{T}$$
 (2)

$$\frac{\hat{s}^{\circ}}{R_{u}} = \frac{s^{\circ}}{R} = a_{1} \ln T + a_{2}T + \frac{a_{3}}{2}T^{2} + \frac{a_{4}}{3}T^{3} + \frac{a_{5}}{4}T^{4} + a_{7}$$
(3)

Note that all the parameters on the left hand side of equations (1) through (3) are dimensionless.

Three temperatures are given on the first line of the data, T_{low} , T_{high} , and T_{mid} . Usually, these values are 300, 5000, and 1000 K respectively. The first set of parameters a_1 through a_7 applies for the high temperature range (T_{mid} through T_{high}), while the second set applies for the low temperature range (T_{low} through T_{mid}).

Sample Data in Chemkin Format for Nitrogen (N₂)

N2	121286N 2	G	0300.00 5000.00 10	00.00	1
0.02926640E + 02	0.14879768E- 02	-0.05684760E -05	0.10097038 E-09	-0.06753351E-13	2
-0.09227977E+04	0.05980528E+02	0.03298677E + 02	0.14082404 E-02	-0.03963222E-04	3
0.05641515 E-07	-0.02444854E-10	-0.10208999E+04	0.03950372E+02		4

Format:

Symbol	Identifier #atoms	Phase	$T_{\rm low}$ $T_{\rm high}$	$T_{ m mid}$	1
a_1 (hi range)	a_2 (hi range)	a_3 (hi range)	a_4 (hi range)	a_5 (hi range)	2
a_6 (hi range)	a_7 (hi range)	a_1 (lo range)	a_2 (lo range)	a_3 (lo range)	3
a_4 (lo range)	a_5 (lo range)	a_6 (lo range)	a_7 (lo range)		4

Equilibrium Example: $O_2 \rightarrow 2O$ Composition at 3000 K and 0.1 and 1 atm. Crunching the numbers.

Data Files in Chemkin Format

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     2.56942078E + 00 - 8.59741137E - 05 \quad 4.19484589E - 08 - 1.00177799E - 11 \quad 1.22833691E - 15 \quad 1.00177799E - 11 \quad 1.22833691E - 15 \quad 1.00177799E - 11 \quad 1.0017799E - 11 \quad 1.001799E - 11 \quad 1.001799E
     2.92175791E+04 4.78433864E+00 3.16826710E+00-3.27931884E-03 6.64306396E-06
-6.12806624E-09 2.11265971E-12 2.91222592E+04 2.05193346E+00 6.72540300E+03
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    3.28253784E+00 1.48308754E-03-7.57966669E-07 2.09470555E-10-2.16717794E-14
-1.08845772E+03 5.45323129E+00 3.78245636E+00-2.99673416E-03 9.84730201E-06
-9.68129509E-09 3.24372837E-12-1.06394356E+03 3.65767573E+00 8.68010400E+03
```

Molar specific heat at constant pressure (J/mol-K): O₂, 39.994; O, 20.935

Molar enthalpy (kJ/mol): O₂, 98.10; O, 305.73

Molar entropy @ 1 atm (J/mol-K): O₂, 284.4987; O, 209.6926

Molar Gibbs Free Energy @ 1 atm (kJ/mol): O₂,-755.39; O, -323.34

Enthalpy of Formation @ 1 atm, 298 K: O₂, 0; O, 249.16

$$\Delta G^{\circ} = 2\hat{\mu}_{O} - \hat{\mu}_{O2} = +108.71 \text{ kJ/mol} \quad K_{p} = \exp(-\Delta G^{\circ}/RT) = 0.0128,$$

using .008314 kJ/mol-K for R, and 3000 K for T.

$$\xi = \sqrt{\frac{K_p}{4(P/P_{ref}) + K_p}}$$

For 1 atm,
$$P = P_{ref}$$
, and $\xi = 0.0565$. $Xo = No/NT = 2\xi/(1 + \xi) = 0.1069$

For 0.1 atm, P/P_{ref} = 0.1, and ξ = 0.1761. Xo = No/NT = 2 ξ /(1+ ξ) = 0.2994

Sample Problem Using Multiple Reactions

K. Consider CO, CO₂, O₂, and O as the possible species.

book, published papers, etc.) and compare results.

tabulated data.

For a mixture of 1 mole of CO and 1 mole of O₂, it is desired to know the equilibrium composition at 3000

a) Choose an appropriate set of reactions and calculate K_p for each reaction at 3000 K from

b) Obtain K_p from another source for the chosen reactions (e.g. a thermo book, a combustion

c) Calculate the equilibrium composition of a mixture of 1 mole CO and 1 mole O₂ at 3000 K

and 1 atm. Give your results in the form of mole fractions for each species.

d) Repeat part c) for P = 0.1 atm. Solution

For parts a) and b) the answers depend on what set of reactions that were chosen. For each reaction, $K_p = \exp\left(-\Delta G^{\circ}/\hat{R}T\right)$. $\Delta G^{\circ} = \sum_i \nu_i \hat{\mu}_i^{\circ}$, where $\hat{\mu}_i^{\circ} = \hat{u}_i(T, P_0) + \hat{R}T - T\hat{s}_i(T, P_0)$. The superscript 'o'

denotes that those quantities are evaluated at the reference pressure, which is typically 1 atmosphere. Even though there are 4 species, we can only write two linearly independent reactions. For example:

 $CO + O \rightleftharpoons CO_2$ and $\frac{1}{2}O_2 \rightleftharpoons O$ (1)

I call the advancement for the first reaction
$$\xi_1$$
 and that for the second reaction ξ_2 . Then I can write the relations:

relations: $N_{\rm CO} = 1 - \xi_1$ $N_{\rm CO_2} = \xi_1$ $N_{\rm O} = \xi_2 - \xi_1$ $N_{\rm O_2} = 1 - \xi_2/2$ (2)

$$N_{\rm CO} = 1 - \xi_1$$
 $N_{\rm CO_2} = \xi_1$ $N_{\rm O} = \xi_2 - \xi_1$ $N_{\rm O_2} = 1 - \xi_2/2$

Also, we note that the total number of moles is the sum over all the species or $N_T = 2 - \xi_1 + \xi_2/2$. These relations tell us that ξ_1 is between 0 and 1 and that ξ_2 is between ξ_1 and 2. Next, we write the expression

for the equilibrium constants for these reactions. For the first reaction, $K_{p,1} = 27.16$ and for the second,

$$K_{p,2} = .1125$$
 at 3000 K (from an undergraduate thermodynamics text).
$$K_{p,1} = \frac{P_{\text{CO}_2}/P_0}{P_{\text{CO}_2}P_0/P_2^2} = \frac{X_{\text{CO}_2}}{X_{\text{CO}_2}X_0} \left(\frac{P_0}{P}\right) = \frac{N_T N_{\text{CO}_2}}{N_{\text{CO}_2}N_0} \left(\frac{P_0}{P}\right)$$

$$X_i = N_i / N_{T_i}$$
. Plugging in our relations for the N's gives us:

Where we have used the fact that $X_i = N_i/N_T$. Plugging in our relations for the N's gives us:

$$K_{p,1} = \frac{(2 - \xi_1 + \xi_2/2)\xi_1}{(1 - \xi_1)(\xi_2 - \xi_1)} \left(\frac{P_0}{P}\right) \tag{4}$$

(3)

(7)

Similarly for $K_{p,2}$ we get:

fractions as follows:

$$K_{p,2} = \frac{\xi_2 - \xi_1}{(2 - \xi_1 + \xi_2/2)^{1/2} (1 - \xi_2/2)^{1/2}} \left(\frac{P}{P_0}\right)^{1/2} \tag{5}$$

Now we have two equations for two unknowns, ξ_1 and ξ_2 . Unfortunately, we can't isolate either variable, so we have to do a systematic search. I chose a value of ξ_1 , and then solved for ξ_2 in $K_{p,2}$ using a Newton-

Raphson method on a calculator. Then I plugged these values into $K_{p,1}$ and used the agreement there as a barometer for convergence. For the P=1 atm case, I got $\xi_1=.646$ and $\xi_2=.763$. This gives me mole

 $X_{CO} = .204$ $X_{CO_2} = .372$ $X_{O} = .067$ $X_{O_2} = .357$ (6)These values agree excellently with those obtained by a canned software routine which solves for equilibrium

These values agree excellently with those obtained by a cannel software routine which solves for equilibrium composition. For the low pressure case,
$$(P/P_0) = 0.1$$
, and I get $\xi_1 = .349$ and $\xi_2 = .749$ leading to the

following mole fractions: $X_{\text{CO}} = .321$ $X_{\text{CO}_2} = .172$ $X_{\text{O}} = .198$ $X_{\text{O}_2} = .309$

$$X_{\rm CO} = .321$$
 $X_{\rm CO_2} = .172$ $X_{\rm O} = .198$ $X_{\rm O_2} = .309$

Note that the reduced pressure has increased N_T as expected due to Le Chatlier's principle.